

Cryopumping – Basics and Applications

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Final version

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Outline

- Introduction.
- Cryopumping mechanisms (condensation, sorption).
- Cryopump sub-systems and issues in their design.
- Commercial cryopumps.
- Tailor-made cryopumps.
- Examples.



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Site of Forschungszentrum Karlsruhe



Institute of

Technical Physics

FZK features three Research Areas:

- Structure of Matter (neutrino mass, ANKA)
- Key Technologies (micro, nano, grid)
- Energy

(fusion, fission, biomass)

FZK: ~ 3500 people

FUSION Programme: ~ 220 FTE

FZK is responsible for 2/3 of the EU Contributions to ITER.

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Pump classification (1)



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Pump classification (2)

1E+5 1E+3 1E+1 1E-1 1E-3 1E-5 1E-7 1E-9 1E-11





Typical pumping speed curve shape



log (Pressure inside the pump)

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Saturation Pressure (Pa)

1E-8

1E-9

1E-10



1E+1

Temperature (K)

1E+2

20K 27K 77K

LH2 LNe LN2

Cryopumping – How does it work?

Definition according to ISO:

.....A cryopump is a vacuum pump which captures the gas by surfaces cooled to temperatures below 120 K

Cryopumps exploit the most elementary form of producing vacuum by lowering the temperature. They are capture pumps which remove gas molecules by sorption or condensation/resublimation.

Pumping of helium, hydrogen?

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1E-1

1E+0

4. 2K

LHe

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1E+3

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Limits of Cryocondensation: Hydrogen as example



Thermodynamic equilibrium → Net pumping speed of Zero

Rule of thumb in design: oversaturation by two decades in pressure



→ For
$$D_2$$
: $p_{eff}(T=4,2K) = 10^{-4} Pa$
okay for $D_2! O^{-4} Pa$



Efficiency of cryocondensation is close to the theoretical maximum, i.e. practically all particles hitting the pumping cryosurface are pumped.



Use of Cryosorption to pump H₂ and He @ 4.2 K

Pumping of the gas via physisorption at the cold cryosorbent. The pumping effect is given by the porosity of the material (pore size distribution rather than BET surface).

- → Zeolites (molecular sieve)
- → Activated charcoal
- → Sintered metal
- \rightarrow Porous ceramics
- → Condensed gas frost (most commonly argon)

The porous materials are bonded to the cooled surfaces (by means of a glue/cement/braze/...).

Additional design parameter: Not only pressure and temperature, but also the gas load \rightarrow saturation effects.



<u>Charcoal is the</u> <u>Standard material</u>



slide # 9



Operation point of the cryosorption pump is given by the sorption isotherms

hydrogen on charcoal

helium on charcoal



The efficiency of cryosorption is lower than for condensation (you need more hits before the particle becomes immobilized), but the achievable equilibrium pressures are always lower, e.g. H_2 : $p=10^{-4}$ Pa: T(eq)=20 K.

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Cryosorbent Material Assessment

Qualification of new Materials and Quality Assurance of different Manufacturing Batches



Refrigerator cold head allows for all temperatures between 3.5 K and 90 K

Sample holder with activated charcoal

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Cryosorbent Material Assessment – Example charcoal

Microscopic views

Granular, highly activated, hydrophobic activated charcoal (1.2 mm)



1 mm

10 *µ*m

100 µm

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Choice for the 'best' cryosorption material: He @ 5K



The optimum material is not only given by sorption issues, But the complete panel set-up has to be taken into account. The coating may lead to different conclusions for powders/granules/pellets.

What counts is the surface-related capacity, not the mass-related value.

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The elementary features of a cryopump set-up: Baffles + shields, pumping panels, and cryosupply





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in-vessel



 $Q_F \sim$

Gas Heat Conduction

2.

Cryopump elements are given by cryogenic issues

$$\dot{Q}_{tot} = \dot{Q}_F + \dot{Q}_G + \dot{Q}_{Rad} + \Delta \dot{H} = \min.$$
1. Solid heat conduction
 $\dot{Q}_F \sim \lambda/L \cdot A \cdot \Delta T$
2. Residual gas heat conduction

$$\int_{u_1} \int_{u_2} \int_{u_1} \int_{u_2} \int_{u_1} \int_{u_2} \int_{u_1} \int_{u_2} \int_{u_1} \int_{u_2} \int_{u_2$$

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cryopumps

10-5

0,8

----- a

09

07

0.6

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Source: Haefer



Consequences

Cryopumps can in principle provide the maximum theoretical ('black hole') pumping speed S_{id}, if the cold surfaces are installed directly in the vacuum recipient (i.e. without any conductance limiting flanges).

However, the baffles which are needed due to cryogenic reasons reduce the pumping speed to the practically achievable value. That reduction is being described by the capture probability c < 1:

$$S = c \cdot S_{id} = c \cdot \sqrt{\frac{R \cdot T}{2 \cdot \pi \cdot M}} \cdot A$$

The ideal pumping speed is reduced for a real pump

- first by the limited *transmission probability w* of a particle on the way from the vessel volume on the pumping surface →
- then by a non 100% *sticking probability* α of a particle at the pumping surface.

That means, in addition to the usually given values for molecular mass M of the gas being pumped, temperature T, and the inlet cross-section A:

The essential design task is to tailor the capture probability function $c \rightarrow max$; Different pump <u>designs</u> should be judged via the parameter c, and not directly via S.

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Contributions to c

Separation of the contributions for a simple geometry: С W Influence of the pumping 0.8 Sticking coefficient 0.6 0.7 mechanism (big or small values, for H2 Geometry sorption a complicated function of influence the pumping history) (constant) He Transmission probability w of the particle from pump inlet to the pumping surface 0 6 5 0,4 1,0 0,8 0.3 θ = 60° 45° 2 10,5 0 30°. 0,2 $\theta = 60^{\circ}$ 1.5 ۸ -≩ 04 30° Monte Carlo-Werte 0,1 Monte Cario-Werte 0.5 0,2 experimentelle Wertel für experimentelle Werte für $\theta = 50^{\circ}$ $\theta = 60^{\circ}$

Sticking coefficient α



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6

8

10 Source: Haefer

<u>4</u>5°

30°

A/B

ŋ



Я

10

45°

3а

A/B

5

2



Liquid He bath cryopump



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The commercial refrigerator cryopump





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The commercial refrigerator cryopump: set-up





The commercial refrigerator cryopump: parameters



Water

$$\begin{split} S_{id} = & 14.9 \ l/(s \cdot cm^2) \ @ \ 300 \ K \\ w = & 1, \ \alpha = & 1 \ \Rightarrow \ c = & 1 \\ S = & S_{id} = & 14.9 \ l/(s \cdot cm^2) \ (Black \ hole \ pumping \ speed) \end{split}$$

Nitrogen

S_{id}=11.9 l/(s·cm²) @ 300 K W=0.25, α=1 → c=0.25 S=0.25·S_{id}=3 l/(s·cm²)

Cryosorbed Gas

H₂: S_{id}=44.6 l/(s·cm²) @ 300 K He: S_{id}=31.5 l/(s·cm²) @ 300 K

H₂: w=0.25, α=0.6 → c=0.21

$$S=0.21 \cdot S_{id}=9.3 \ l/(s \cdot cm^2)$$

He: w=0.25, α=0.3 → c=0.16
 $S=0.16 \cdot S_{id}=5 \ l/(s \cdot cm^2)$



Standardised criteria for refrigerator-cooled cryopumps

		LAUNPIC DIN SEO
		10000 L/s (water)
1.	Pumping speed	3000 L/s (air)
2. 3.	Maximum throughput Pumping capacity:	~ 2 Pam³/s (Ar)
	\rightarrow The pumping speed decreases with an increasing amount of pumped gas. Especially for adsorbed gases, the pumping speed	
	asymptotically reaches zero. To have a comparable and	
	reproducible measure, the pumping capacity is defined as the quantity of gas, which has been pumped until pumping speed	10 ⁵ Pam ³ (Ar)
	has been reduced to 50% of the initial value. The test for	10 Pam ³ (He)
	that a decrease of 50% in pumping speed is indicated by	
	doubling the pressure.	10 -10 De
4.	Ultimate pressure (of the baked pump, after 24 hours).	10 ⁻¹⁰ Pa
5.	Cool-down time (from ambient to 100/20 K).	211
6.	Crossover:	
	\rightarrow The crossover is defined by the maximum amount of nitrogen gas, which can be admitted into the pump in a time interval of 3 s, while the second stage remains at temperatures below 20 K	40 Pam ³
	s, while the second stage remains at temperatures below 20 K.	

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Example: DNI 320



What a refrigerator cryopump system comprises





Regeneration

Regeneration of the cryopumps:

- becomes necessary, when the pumping speed has decreased to an inacceptable level (which indicates the achievement of the saturation limit).

- may become necessary even before that point, due to safety reasons when flammable gas has been pumped (hydrogen for example). An air inbreak may cause explosive gas mixtures (oxy-hydrogen explosion), which has to be avoided by a strict inventory limitation so that even under the safety event the concentrations stay below the explosion limit.

Regeneration means:

- Automatic heating or purging with warm gas, Gasrelease (Sublimation, Desorption) and pump-down of the gas via the backing system, or:

- complete exchange of the cold surface unit.



Regeneration: Sublimation vs. desorption \rightarrow re-adsorption

Example CO_2





Regeneration: Typical desorption curves





Other operational effects in cryosorption pumping

- A <u>poisoning effect</u> of the sorbent may appear, i.e. a reduction of the nominal sorption pumping speed due to accumulation of gas species which are not regenerated within the normal regeneration pattern (all strongly sorbed gases such as heavy hydrocarbons). This effect can be mitigated by a suitable choice of the cryosorbent (Ar frost) or by provision of 'extra' regeneration methods.

- <u>Mobility</u> of the sorbed particles plays a role. The capacity of the pump can be increased by defined temperature peaks, which give the sorbed particle at the surface enough energy to migrate deeper into the pores.

- <u>Fractionation</u> of the components when a mixture is being pumped is possible due to the different pumping mechanisms.



Effects 1: Poisoning





Other operational effects in cryosorption pumping

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Effects 2: Mobility



Example D_2



Other operational effects in cryosorption pumping

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Effects 3: Fractionation (1)





Effects 3: Fractionation (2)





Principle pumping speed curves in molecular flow as a function of temperature



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Advantages of Cryopumping (1)

- Cryopumps produce the biggest pumping speeds of all vacuum pumps:
 - → up to 60 m³/s (nitrogen) via DN1200 for commercial pumps (compare with maximum 3 m³/s via DN 300 using turbopumps)
 - → custom-made cryopumps can provide very high pumping speed via the smallest connection area needs (e.g. 100 m³/s (Helium) via DN750).
 - \rightarrow custom-made cryopumps can be installed in situ.
- Cryopumps are absolutely oil-free and generate a clean vacuum completely free of oil or hydrocarbons → optimal for clean applications.
- Cryopumps do not have any movable parts \rightarrow
- No bearing and shaft seal problems (maintenance aspects, lubrication aspects).
 - \rightarrow Stable against electrical blackouts (if cryogen-based).
 - \rightarrow High reliability and no problem with dust and particles.
 - → Compatible with strongest safety requirements, cryogen-based cryopumps are excellent for areas with difficult maintenance access ('build in and forget').
- Cryopumps can be installed in all directions.



Advantages of Cryopumping (2)

- No backing pump system is needed during operation of the cryopump.
- Cryopumps are the pumps of choice for pumping of water/steam or wet gases (extremely high pumping speeds and no corrosion problems).
- The pumping speed of cryopumps increases for light gases.
- Cryopumps are operable over a wide pressure range.
- Cryogen-based cryopumps do not need any electrical power supply at all (which is good for operation under high magnetic fields) and are completely vibration-free.

• ...



Combination of Refrigerator/LN2



- Three stage cryopump.
 - \rightarrow Inlet shield cooled to 77 K with liquid nitrogen.
 - → Inside the pump there is a two-stage GM-refrigerator, which provides 50 K on its first stage for the condensation stage,
 - → and 20 K on ist second stage for the sorption stage (charcoal).
- The regeneration can be done with electrical heaters or purging with warm gas.
- Inlet diameter of 1.25 m
- nominal pumping speed of 50 m³/s for nitrogen (capture coefficient c=0.35) and hydrogen (capture coefficient c=0.09).
- Developed for space simulation chmabers (10⁻⁴ Pa).

Source: Air Liquide



A modular panel approach allows an optimal design for the given geometry





Panel manufacturing



Equipped with temperature sensors





A modular square-shape cryopump with liquid cryogens



Dimension: 4.4 m x 1.5 m Supply with 35-40 g/min LHe And 50 l/h LN2.

Nominal pumping speed for hydrogen is 400 m³/s.



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The three cryopump elements





Starting requirement: Replace a titanium sublimation pump, stay in the available space and increase the Pumping speed by factor 10.

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slide # 41



ITER Vacuum Systems - Outline



slide # 42



ITER Large High Vacuum Cryopump Systems - Overview

		Torus	Beam Heating (NBI)	Cryostat
# Pumps		8	2 (3) +1	2
Pumping mode	<u>Hig</u> l rela → <u>H</u> → <u>Pu</u> tr	Dynamic = maintain the pressure (1- <u>n gas throughput at</u> <u>tively high pressures</u> <u>igh pumpings speeds</u> , <u>igh pumpings speeds</u> , <u>igh pumpings speeds</u> , <u>of</u> <u>ate</u>) <u>ansitional range</u>))+ (33 Pa·m ³ /s (impurities)); Base pressure for hydrogens: 10 ⁻⁵ Pa.	Dynamic = maintain the pressure (0.01 Pa) inside the NBI volume (150 m ³ /H-NBI) at a through These systems as well Rest of ITER will be co Talk by Mike Wykes C	Transient pump-down (closed cryostat volume of 8400 as all the overed in a special on Tuesday.
Gases		Hydrogen (all six isotopes), helium, impurities Depending strongly on the operation mode (burn& dwell, conditioning, leak detection)	Hydrogen (H ₂ , D ₂)	Nitrogen, outgassing gas



Design Issues in the Development of the ITER torus Cryopumps

- Pumping port size is limited → Maximize pumping speed / Capture probability at constant entrance area.
- 2. Worst case to design the cryosorbent panels \rightarrow reference design shall include a pure helium/protium shot (which means 100% sorption pumping).
- The composition of the gas mixture being pumped may vary significantly → Minimize the dependency of pumping speed on gas species.
- The gas throughput is variable and must be controllable → include an inlet valve for control.
- The distance between the pumps⁻ location and the divertor is given and big → Maximize conductance of the pumping port.
- Compatibility with the operating conditions → Magnetic and electric fields, seismic, tritium-compatibility, Safety (Hydrogen explosion), Remote handling....
- 7. Find and characterise the *coptimum* cryosorbent.



Step 1: Operational Scheme for the Torus Cryopump







Staggering Interval given by Inventory Limitation





Step 2: Complete System Flow Analysis





Typical results under plasma burn: Mass influence



Minimum 50 m³/s as target nominal pumping speed per (pump+inlet bellow) \rightarrow This defines the requested pump size !

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Design of the ITER Pump with integrated inlet valve



Valve Diameter	700 mm	
Valve Stroke	400 mm	
Pump Length	1350 mm	
Pump Diameter	1200 mm	
Coated Cryopanel Surface Area:		
16 panels, 4 m ²	2	
Panel Length	870 mm	
Pump volume	1 m³ (+5)	





Experimental Basis: Test of a Torus Model Cryopump in the TIMO Test Bed at FZK











Pumping speed results

Pumping with transitional flow conditions inside the pump.





Gas Species Dependency



Almost insensitive against the type of gas being pumped, Although big differences in $\alpha(\text{He})=0.2 \text{ vs. } \alpha(D_2)=0.9$. Achieved by a sophisticated interior design.



Saturation capacities @ 5K





4000 m³/s cryopump set-up with its three elementary parts





...If you want to read about cryopumps

- The Bible:

R.A. Haefer, Cryopumping, Clarendon Press, Oxford, 1989.

- M. Hablanian, High vacuum technology, 2n ed., Dekker, New York, 1997.
- J.M. Lafferty (Ed.), Foundations of vacuum science and technology, John Wiley, 1998.
- K.M. Welch, Capture pumping technology, 2nd ed., North-Holland Elsevier, Amsterdam, 2003.

Thank you for your attention